Overall Objectives of Model Predictive Control

- 1. Prevent violations of input and output constraints.
- 2. Drive some output variables to their optimal set points, while maintaining other outputs within specified ranges.
- 3. Prevent excessive movement of the input variables.
- 4. If a sensor or actuator is not available, control as much of the process as possible.

Model Predictive Control: Basic Concepts

- 1. Future values of output variables are predicted using a dynamic model of the process and current measurements.
 - Unlike time delay compensation methods, the predictions are made for more than one time delay ahead.
- 2. The control calculations are based on both future predictions and current measurements.
- 3. The manipulated variables, u(k), at the k-th sampling instant are calculated so that they minimize an objective function, J.
 - **Example:** Minimize the sum of the squares of the deviations between predicted future outputs and specific reference trajectory.
 - The reference trajectory is based on set points calculated using RTO.
- 4. Inequality & equality constraints, and measured disturbances are included in the control calculations.
- 5. The calculated manipulated variables are implemented as set point for lower level control loops. (cf. cascade control).

Model Predictive Control: Calculations

- 1. At the *k*-th sampling instant, the values of the manipulated variables, *u*, at the next *M* sampling instants, {*u*(k), *u*(k+1), ..., *u*(k+*M*-1)} are calculated.
 - This set of *M* "control moves" is calculated so as to minimize the predicted deviations from the reference trajectory over the next *P* sampling instants while satisfying the constraints.
 - Typically, an LP or QP problem is solved at each sampling instant.
 - Terminology: M = control horizon, P = prediction horizon
- 2. Then the first "control move", $\mathbf{u}(k)$, is implemented.
- 3. At the next sampling instant, k+1, the M-step control policy is re-calculated for the next M sampling instants, k+1 to k+M, and implement the first control move, $\mathbf{u}(k+1)$.
- 4. Then Steps 1 and 2 are repeated for subsequent sampling instants.

Note: This approach is an example of a *receding horizon* approach.

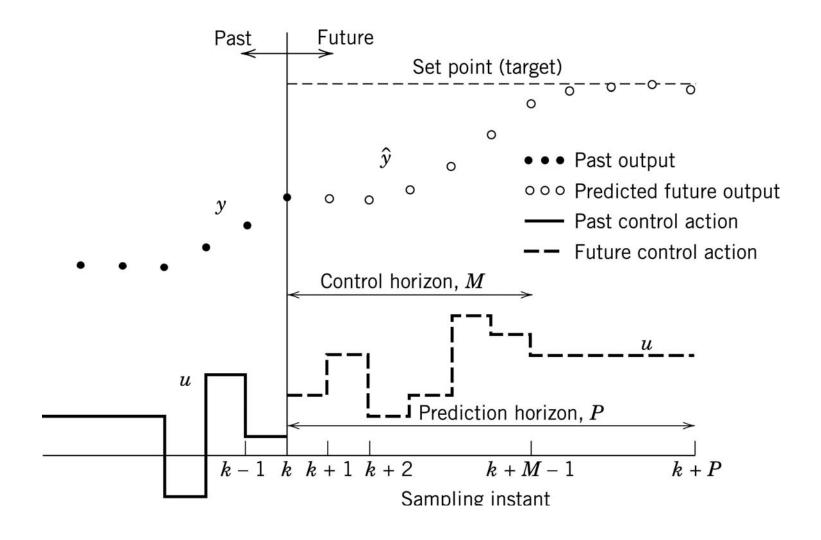


Figure 20.2 Basic concept for Model Predictive Control

When Should Predictive Control be Used?

- Processes are difficult to control with standard PID algorithm (e.g., large time constants, substantial time delays, inverse response, etc.
- 2. There is significant process interactions between **u** and **y**.
 - i.e., more than one manipulated variable has a significant effect on an important process variable.
- 3. Constraints (limits) on process variables and manipulated variables are important for normal control.

Terminology:

• $y \leftrightarrow CV$, $u \leftrightarrow MV$, $d \leftrightarrow DV$

Model Predictive Control Originated in 1980s

- Techniques developed by industry:
 - 1. Dynamic Matrix Control (DMC)
 - Shell Development Co.: Cutler and Ramaker (1980),
 - Cutler later formed DMC, Inc.
 - DMC acquired by Aspentech in 1997.
 - 2. Model Algorithmic Control (MAC)
 - ADERSA/GERBIOS, Richalet et al. (1978) in France.
- Over 5000 applications of MPC since 1980

Reference: Qin and Badgwell, 1998 and 2003).

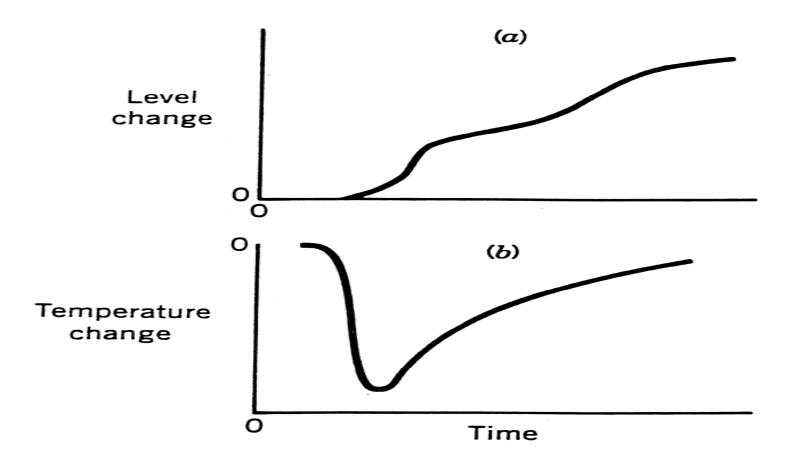


Figure A. Two processes exhibiting unusual dynamic behavior.

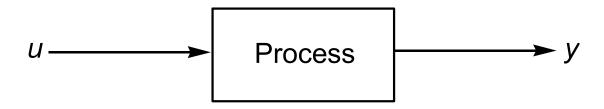
- (a) change in base level due to a step change in feed rate to a distillation column.
- (b) steam temperature change due to switching on soot blower in a boiler.

Dynamic Models for Model Predictive Control

- Could be either:
 - 1. Physical or empirical (but usually empirical)
 - 2. Linear or nonlinear (but usually linear)
- Typical linear models used in MPC:
 - 1. Step response models
 - 2. Transfer function models
 - 3. State-space models
- Note: Can convert one type of linear model (above) to the other types.

Discrete Step Response Models

Consider a single input, single output process:



where *u* and *y* are deviation variables (i.e., deviations from nominal steady-state values).

Prediction for SISO Models:

Example: Step response model

$$y(k+1) = y_0 + \sum_{i=1}^{N-1} S_i \Delta u(k-i+1) + S_N u(k-N+1)$$
 (20-1)

 S_i = the *i*-th step response coefficient

N =an integer (the *model horizon*)

 y_0 = initial value at k=0

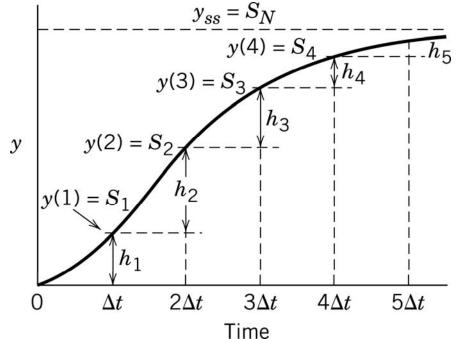


Figure 7.14. Unit Step Response

Prediction for SISO Models:

Example: Step response model

$$y(k+1) = y_0 + \sum_{i=1}^{N-1} S_i \Delta u(k-i+1) + S_N u(k-N+1)$$
 (20-1)

• If y_0 =0, this one-step-ahead prediction can be obtained from Eq. (20-1) by replacing y(k+1) with $\hat{y}(k+1)$

$$\hat{y}(k+1) = \sum_{i=1}^{N-1} S_i \Delta u(k-i+1) + S_N u(k-N+1)$$
 (20-6)

• Equation (20-6) can be expanded as:

$$\hat{y}(k+1) = \underbrace{S_1 \Delta u(k)}_{Effect \ of \ current \ control \ action} + \underbrace{\sum_{i=2}^{N-1} S_i \Delta u(k-i+1) + S_N \ u(k-N+1)}_{Effect \ of \ past \ control \ actions}$$

Prediction for SISO Models: (continued)

Similarly, the j-th step ahead prediction is Eq. 20-10:

$$\hat{y}(k+j) = \sum_{i=1}^{j} S_i \Delta u(k+j-i) + \sum_{i=j+1}^{N-1} S_i \Delta u(k+j-i) + S_N u(k+j-N)$$
Effects of current and future control actions
$$Effects of past control actions$$

Define the predicted unforced response as:

$$\hat{y}^{o}(k+j) \triangleq \sum_{i=j+1}^{N-1} S_{i} \Delta u(k+j-i) + S_{N} u(k+j-N)$$
 (20-11)

and can write Eq. (20-10) as:

$$\hat{y}(k+j) = \sum_{i=1}^{J} S_i \Delta u(k+j-i) + \hat{y}^o(k+j)$$
 (20-12)

Vector Notation for Predictions

Define vectors:

$$\hat{Y}(k+1) \triangleq col[\hat{y}(k+1), \hat{y}(k+2), ..., \hat{y}(k+P)]$$
 (20-16)

$$\hat{\mathbf{Y}}^{o}(k+1) \triangleq col[\hat{y}^{o}(k+1), \hat{y}^{o}(k+2), ..., \hat{y}^{o}(k+P)] \quad (20-17)$$

$$\Delta U(k) \triangleq col \left[\Delta u(k), \Delta u(k+1), \cdots, \Delta u(k+M-1) \right] \qquad (20-18)$$

The model predictions in Eq. (20-12) can be written as:

$$\hat{\mathbf{Y}}(k+1) = \mathbf{S}\Delta \mathbf{U}(k) + \hat{\mathbf{Y}}^{o}(k+1) \qquad (20-19)$$

Dynamic Matrix Model

The model predictions in Eq. (20-12) can be written as:

$$\hat{Y}(k+1) = S\Delta U(k) + \hat{Y}^{o}(k+1) \qquad (20-19)$$

where S is the $P \times M$ dynamic matrix:

$$S \triangleq \begin{bmatrix} S_{I} & 0 & \cdots & 0 \\ S_{2} & S_{I} & 0 & \vdots \\ \vdots & \vdots & \ddots & 0 \\ S_{M} & S_{M-1} & \cdots & S_{I} \\ S_{M+I} & S_{M} & \cdots & S_{2} \\ \vdots & \vdots & \ddots & \vdots \\ S_{P} & S_{P-I} & \cdots & S_{P-M+I} \end{bmatrix}$$
 (20-20)

Bias Correction

- The model predictions can be corrected by utilizing the latest measurement, y(k).
- The *corrected prediction* is defined to be:

$$\tilde{y}(k+j) \triangleq \hat{y}(k+j) + [y(k) - \hat{y}(k)]$$
 (20-23)

• Similarly, adding this bias correction to each prediction in (20-19) gives:

$$\tilde{Y}(k+1) = S\Delta U(k) + \hat{Y}^{o}(k+1) + [y(k) - \hat{y}(k)]I$$
 (20-24)

where $\tilde{Y}(k+1)$ is defined as:

$$\tilde{\mathbf{Y}}(k+1) \triangleq col\left[\tilde{\mathbf{y}}(k+1), \tilde{\mathbf{y}}(k+2), \dots, \tilde{\mathbf{y}}(k+P)\right] \quad (20-25)$$

EXAMPLE 20.4

The benefits of using corrected predictions will be illustrated by a simple example, the first-order plus-time-delay model of Example 20.1:

$$\frac{Y(s)}{U(s)} = \frac{5e^{-2s}}{15s+1} \tag{20-26}$$

Assume that the disturbance transfer function is identical to the process transfer function, $G_d(s) = G_p(s)$. A unit step change in u occurs at time t=2 min and a step disturbance, d=0.15, occurs at t=8 min. The sampling period is $\Delta t=1$ min.

- (a) Compare the process response y(k) with the predictions that were made 15 steps earlier based on a step response model with N=80. Consider both the corrected prediction
- (b) Repeat part (a) for the situation where the step response coefficients are calculated using an incorrect model:

$$\frac{Y(s)}{U(s)} = \frac{4e^{-2s}}{20s+1} \tag{20-27}$$

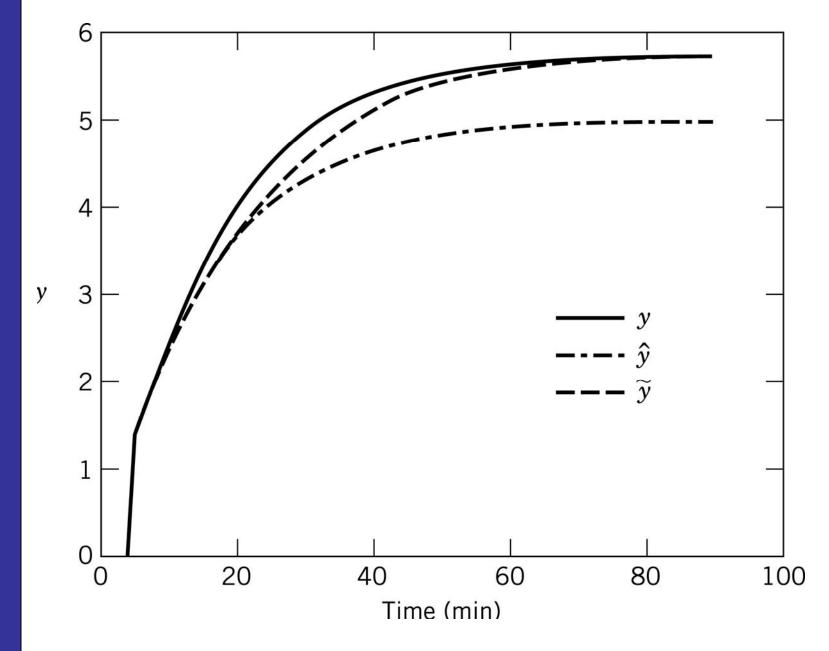


Figure 20.6 Without model error.

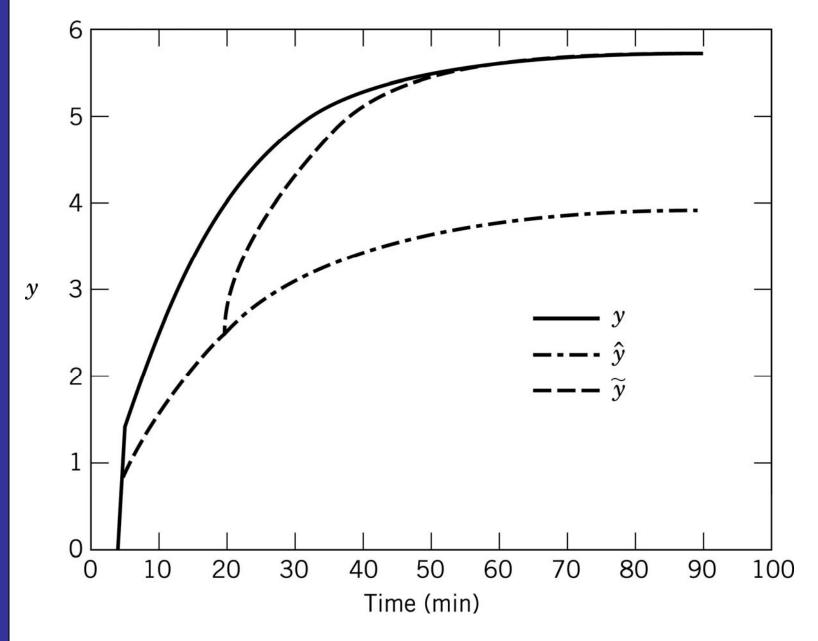


Figure 20.7 With model error.

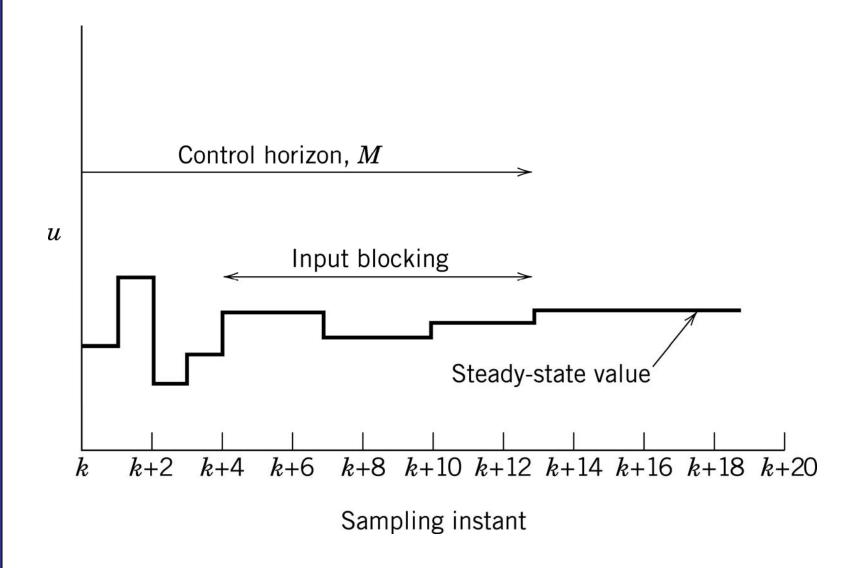


Figure 20.10 Input blocking.

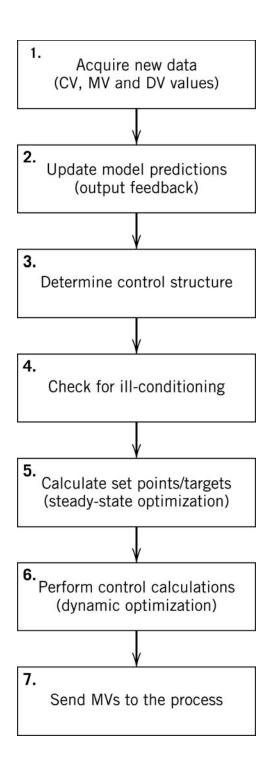


Figure 20.9 Flow chart for MPC calculations.

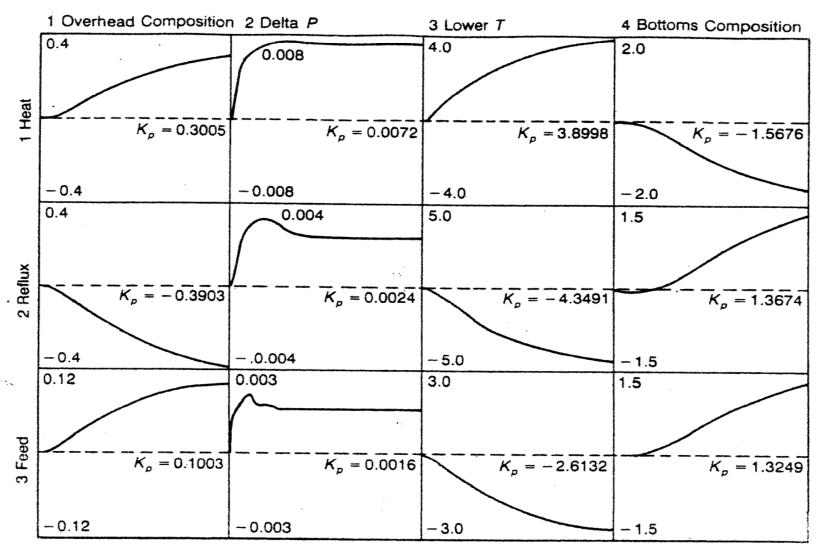


Figure 20.8. Individual step-response models for a distillation column with three inputs and four outputs. Each model represents the step response for 120 minutes. Reference: Hokanson and Gerstle (1992).

Reference Trajectory for MPC

Reference Trajectory

- A reference trajectory can be used to make a gradual transition to the desired set point.
- The reference trajectory Y_r can be specified in several different ways. Let the reference trajectory over the prediction horizon P be denoted as:

$$Y_r(k+1) \triangleq col[y_r(k+1), y_r(k+2), ..., y_r(k+P)]$$
 (20-47)

where Y_r is an mP vector where m is the number of outputs.

Exponential Trajectory from y(k) to $y_{sp}(k)$

A reasonable approach for the *i*-th output is to use:

$$y_{i,r}(k+j) = (a_i)^j y_i(k) + [1 - (a_i)^j] y_{i,sp}(k)$$
 (20-48)

for
$$i=1,2,...,m$$
 and $j=1,2,...,P$.

MPC Control Calculations

- The control calculations are based on minimizing the predicted deviations between the reference trajectory.
- The *predicted error* is defined as:

$$\hat{\boldsymbol{E}}(k+1) \triangleq \boldsymbol{Y}_{r}(k+1) - \tilde{\boldsymbol{Y}}(k+1) \tag{20-50}$$

where $\tilde{Y}(k+1)$ is the corrected prediction defined in (20-37). Similarly, the *predicted unforced error*, $\hat{E}^{o}(k+1)$, is defined as:

$$\hat{\boldsymbol{E}}^{\mathrm{o}}(k+1) \triangleq \boldsymbol{Y}_{r}(k+1) - \tilde{\boldsymbol{Y}}^{\mathrm{o}}(k+1) \tag{20-51}$$

- Note that all of the above vectors are of dimension, mP.
- The objective of the control calculations is to calculate the control policy for the next *M* time intervals:

$$\Delta U(k) \triangleq col[\Delta u(k), \Delta u(k+1), \cdots, \Delta u(k+M-1)] \quad (20-18)$$

MPC Performance Index

- The rM-dimensional vector $\Delta U(k)$ is calculated so as to minimize:
 - a. The predicted errors over the prediction horizon, P.
 - b. The size of the control move over the control horizon, M.
- **Example:** Consider a quadratic performance index:

$$\min_{\Delta U(k)} \mathbf{J} = \hat{\mathbf{E}}(k+1)^T \mathbf{Q} \,\hat{\mathbf{E}}(k+1) + \Delta \mathbf{U}(k)^T \,\mathbf{R} \,\Delta \mathbf{U}(k)$$
(20-54)

where Q is a positive-definite weighting matrix and R is a positive semi-definite matrix.

Both Q and R are usually diagonal matrices with positive diagonal elements.

The weighting matrices are used to weight the most important outputs and inputs (cf. Section 20.6).

MPC Control Law: Unconstrained Case

•The MPC control law that minimizes the objective function in Eq. (20-54) can be calculated analytically,

$$\Delta U(k) = (S^T Q S + R)^{-1} S^T Q \hat{E}^{o}(k+1) \qquad (20-55)$$

where S is the dynamic matrix defined in (20-41).

• This control law can be written in a more compact form,

$$\Delta U(k) = K_c \hat{E}^{o}(k+1) \tag{20-56}$$

where controller gain matrix K_c is defined to be:

$$\boldsymbol{K}_{c} \triangleq (\boldsymbol{S}^{T} \boldsymbol{Q} \ \boldsymbol{S} + \boldsymbol{R})^{-1} \boldsymbol{S}^{T} \boldsymbol{Q} \tag{20-57}$$

- Note that K_c can be evaluated off-line, rather than on-line, provided that the dynamic matrix S and weighting matrices, Q and R, are constant.
- The calculation of K_c requires the inversion of an $rM \times rM$ matrix where r is the number of input variables and M is the control horizon.

MPC Control Law: Receding Horizon Approach

MPC control law:

$$\Delta U(k) = K_c \hat{E}^{o}(k+1) \tag{20-56}$$

where:

$$\Delta U(k) \triangleq col[\Delta u(k), \Delta u(k+1), \cdots, \Delta u(k+M-1)] \quad (20-18)$$

- Note that the controller gain matrix, K_c , is an $rM \times mP$ matrix.
- In the *receding horizon control* approach, only the first step of the M-step control policy, $\Delta u(k)$, in (20-18) is implemented.

$$\Delta u(k) = \mathbf{K}_{cl} \hat{\mathbf{E}}^{o}(k+1) \tag{20-58}$$

where matrix K_{cl} is defined to be the first r rows of K_c . Thus, K_{cl} has dimensions of $r \times mP$.

Selection of Design Parameters

Model predictive control techniques include a number of design parameters:

N: model horizon

 Δt : sampling period

P: prediction horizon (number of predictions)

M: control horizon (number of control moves)

Q: weighting matrix for predicted errors (Q > 0)

R: weighting matrix for control moves $(\mathbf{R} \ge 0)$

Selection of Design Parameters (continued)

1. N and Δt

These parameters should be selected so that $N \Delta t \ge$ open-loop settling time. Typical values of N:

$$30 \le N \le 120$$

2. Prediction Horizon, P

Increasing P results in less aggressive control action

Set
$$P = N + M$$

3. Control Horizon, M

Increasing *M* makes the controller more aggressive and increases computational effort, typically:

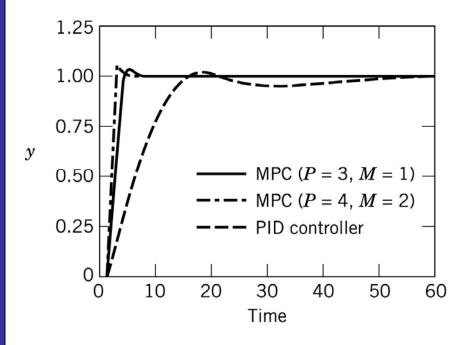
$$5 \le M \le 20$$

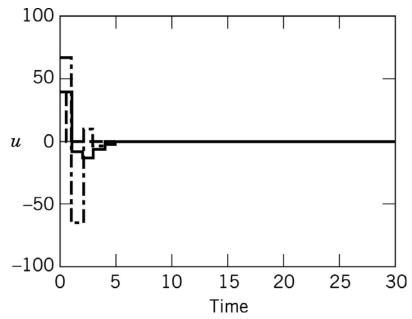
4. Weighting matrices Q and R

Diagonal matrices with largest elements corresponding to most important variables

Example 20.5: set-point responses

$$G(s) = \frac{e^{-s}}{(10 s + 1)(5s + 1)}$$





Example 20.5: disturbance responses

